

Clean hydrogen production from electro-reforming of oxygenated organic compounds

C. Coutanceau,

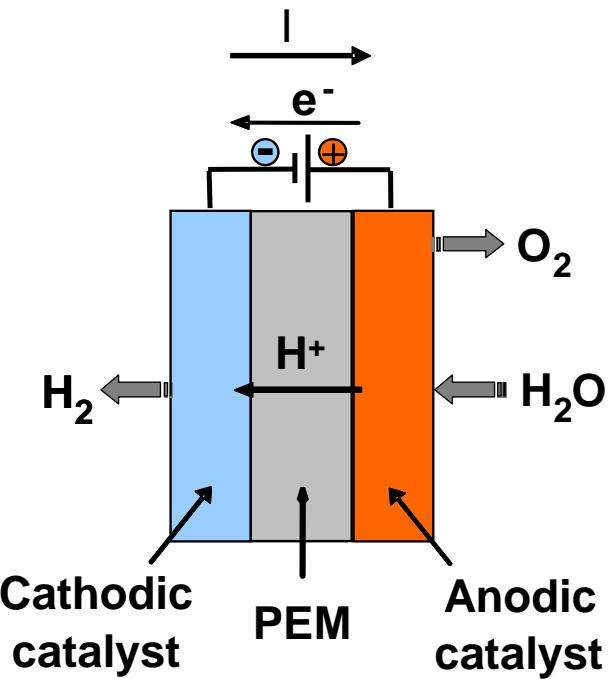
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Co-responsible of the "Stationary Applications" of FRH2 CNRS n° 2044

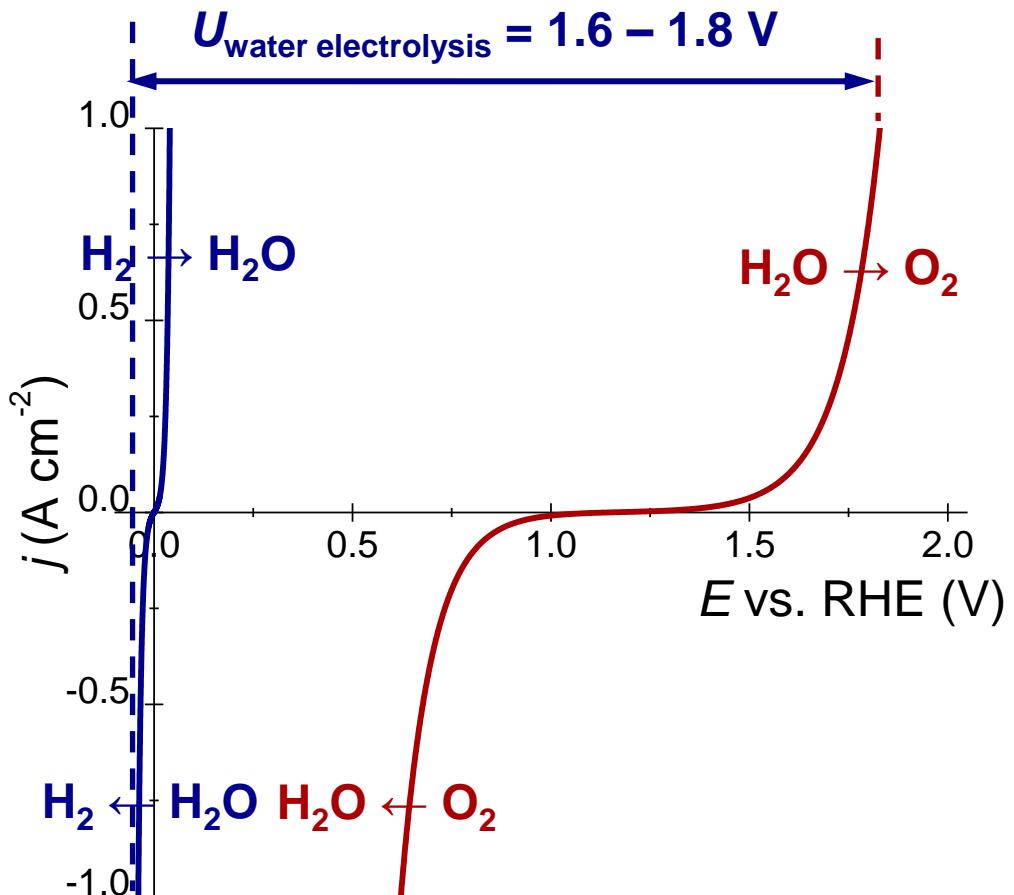
Co-responsible "Catalysis and Non-conventional Media" group of IC2MP
UMR CNRS-University of Poitiers n° 7285

Project manager at the "Energie hub" of CNRS

Water electrolysis



Overall reaction
 $\text{H}_2\text{O} \rightarrow \text{H}_2 + \frac{1}{2}\text{O}_2$



$$W_e \text{ (in kWh/Nm}^3) = \frac{n_e F}{3600 V_m \times 10^3} U_{\text{cell}}(j) \approx 2.364 U_{\text{cell}}(j)$$

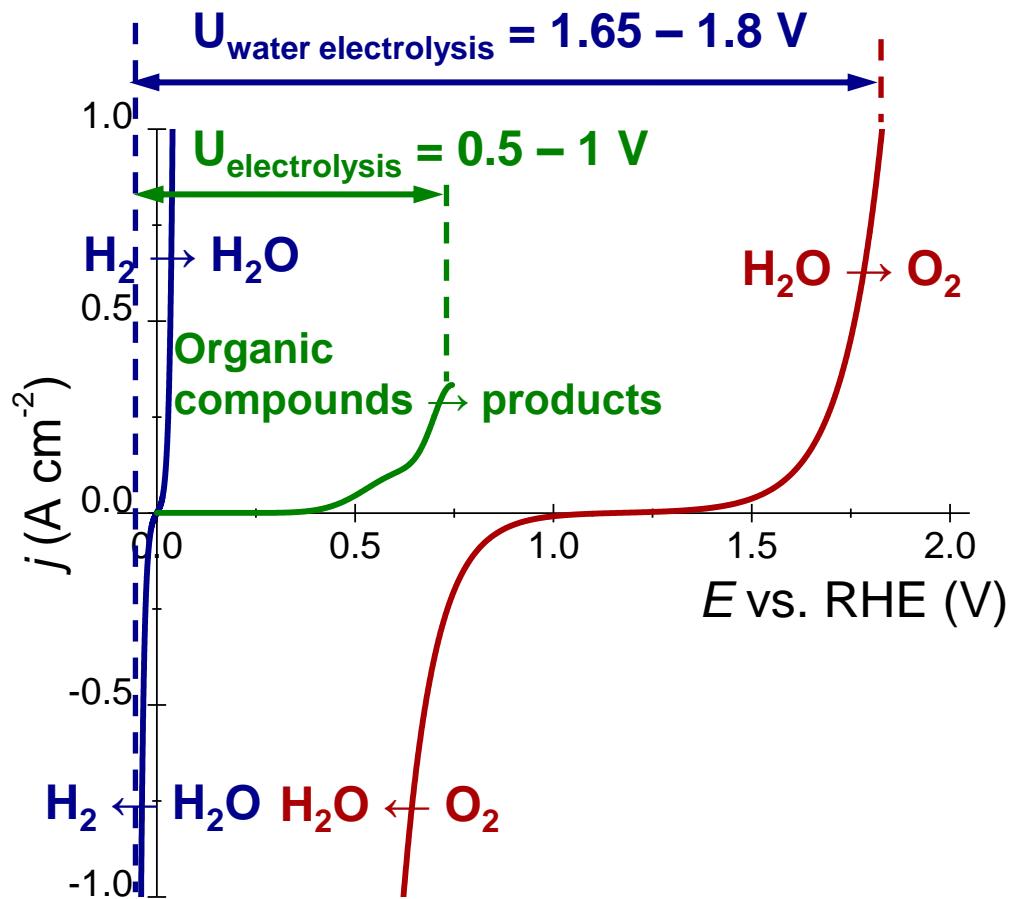
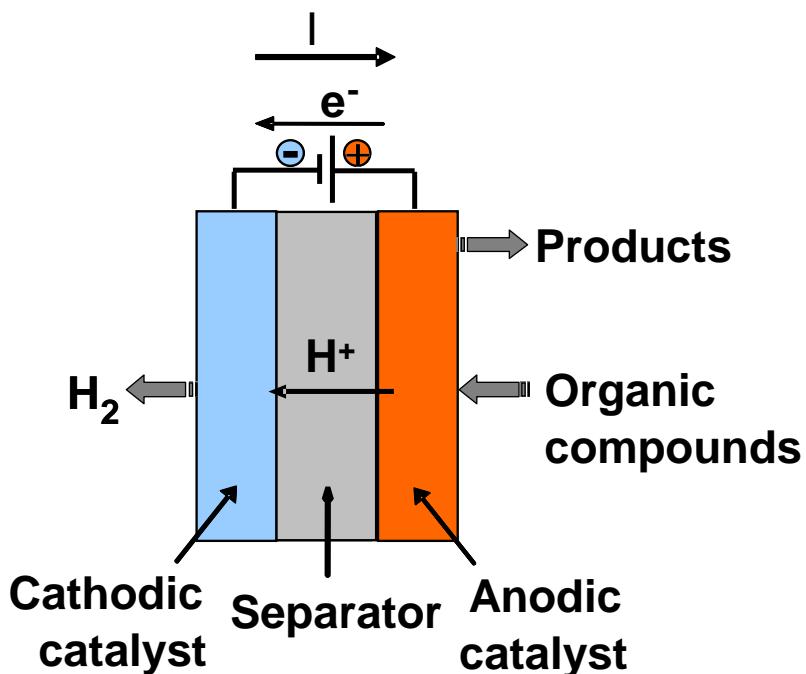
$$W_e = 3.8 - 4.3 \text{ kWh / sm}^3$$

Water electrolysis vs. electroreforming of oxygenated compounds

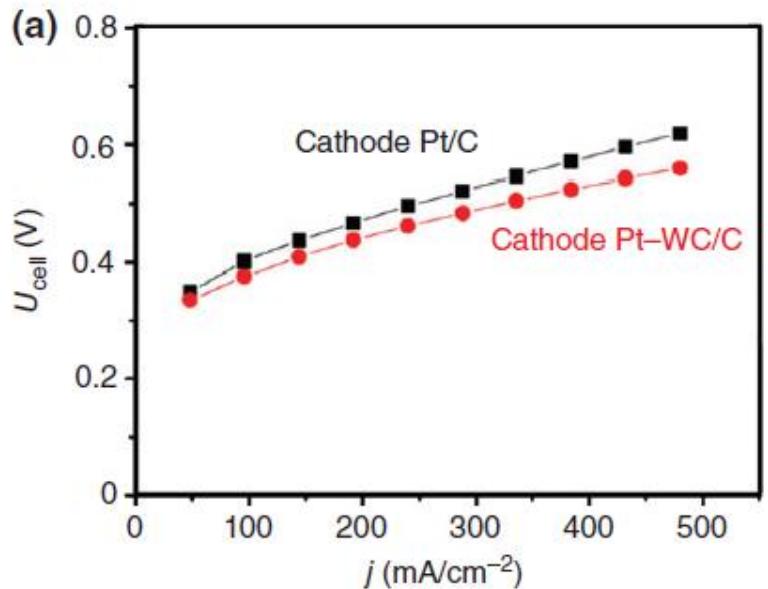
| Compound | n_{H_2} / mole | ΔH^{+0} / kJ mol $^{-1}$ | Δh^{+0} / kJ mol H $_2$ $^{-1}$ | ΔG^{+0} / kJ mol $^{-1}$ | $U_{cell}^0 \approx$ $+ \Delta G^{+0}/nF$ (V vs. SHE) |
|---------------------------------|---------------------|-------------------------------------|--|-------------------------------------|---|
| H $_2$ O | 1 | + 286 | + 286 | + 237 | 1.23 |
| HCOOH | 1 | + 32 | + 32 | - 33 | - 0.17 |
| CH $_3$ OH | 3 | + 131.2 | + 44 | + 9.3 | 0.016 |
| C $_2$ H $_5$ OH | 6 | + 348 | + 58 | + 97.3 | 0.084 |
| CH $_2$ OH-CH $_2$ OH | 5 | + 240 | + 48 | + 17.2 | 0.018 |
| 1-C $_3$ H $_7$ OH | 9 | + 545 | + 61 | + 170 | 0.098 |
| DMM CH $_2$ (OCH $_3$) $_2$ | 8 | + 340.6 | + 42.6 | - 5.6 | - 0.004 |
| CH $_2$ OH-CHOH-CH $_2$ OH | 7 | + 350 | + 50 | - 1 | - 0.001 |
| 1-C $_4$ H $_9$ OH | 12 | + 754 | + 63 | + 205 | 0.177 |
| Glucose | 12 | + 627.1 | + 52.3 | - 27.4 | - 0.012 |

C. Lamy, C. Coutanceau, S. Baranton, Production of clean hydrogen by electrochemical reforming of oxygenated organic compounds, in "Hydrogen Energy and Fuel Cells Primers", B. Pollet (Ed.), Elsevier, Amsterdam, 2020. ISBN: 978-0-12-821500-5.

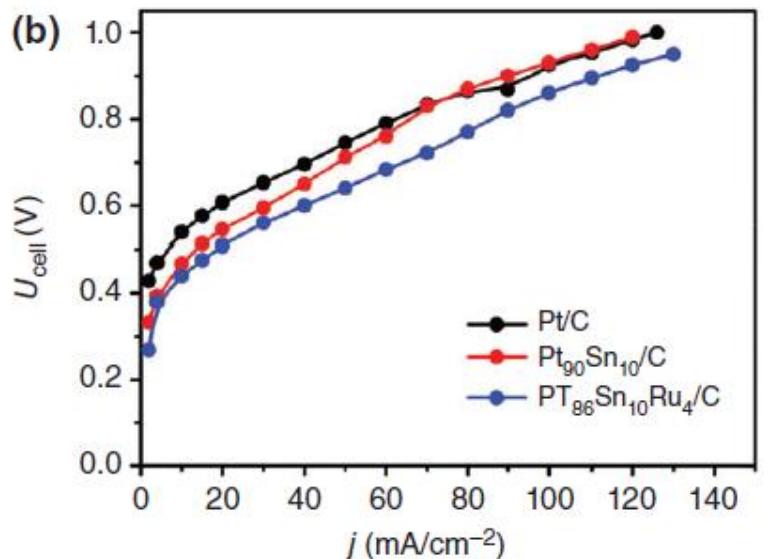
Co-production of **high purity H₂** and **value-added products**



$$W_e = 1.2 - 2.4 \text{ kWh / sm}^3$$



Electrolysis cell voltage versus current density $U_{cell}(j)$ for the oxidation in proton exchange membrane electrolysis cells (PEMEC)



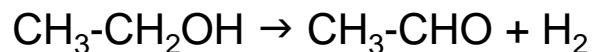
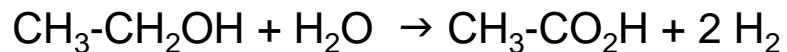
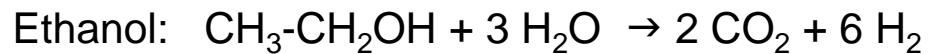
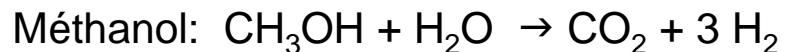
(a) 2 M MeOH (anode PtRu/C) at 90°C

Hu Z, Wu M, Wei Z, Songa S, Shen PK. Pt-WC/C as a cathode electrocatalyst for hydrogen production by methanol electrolysis. *J Power Sources* 166 (2007) 458–461.

(b) 2 M EtOH (cathode Pt/C) at 20°C.

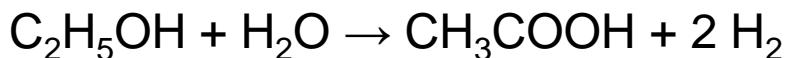
Lamy C, Jaubert T, Baranton S, Coutanceau C. Clean hydrogen generation through the electrocatalytic oxidation of ethanol in a proton exchange membrane electrolysis cell (PEMEC). Effect of the nature and structure of the catalytic anode. *J Power Sources* 245 (2014) 927–936.

Reactions in a Direct Alcohol Proton Exchange Membrane Electrolysis Cell



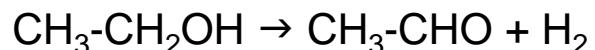
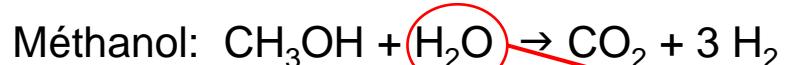
C. Coutanceau, S. Baranton. Electrochemical conversion of alcohols for hydrogen production: a short overview. *WIREs Energy Environ* 2016. doi: 10.1002/wene.193

| Catalyst | AL | AA | CO_2 | Calculated $n_e^{(*)}$ |
|--|-------------------------------|-----------|---------------|---------------------------|
| Pt / C | $U_{\text{cell}} / \text{V}$ | | 0.92 – 0.97 | 3.5 |
| | Chemical yield / mol % | 46 | 42 | |
| $\text{Pt}_{0.9}\text{Sn}_{0.1} / \text{C}$ | $U_{\text{cell}} / \text{V}$ | | 0.92 – 0.97 | 4.6 |
| | Chemical yield / mol % | 31 | 41 | |
| $\text{Pt}_{0.86}\text{Sn}_{0.1}\text{Ru}_{0.04} / \text{C}$ | $U_{\text{cell}} / \text{V}$ | | 0.80 – 0.96 | 4.5 |
| | Chemical yield / mol % | 39 | 32 | |



Electroreforming of oxygenated compounds

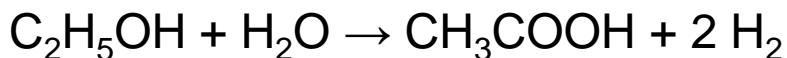
Reactions in a Direct Alcohol Proton Exchange Membrane Electrolysis Cell



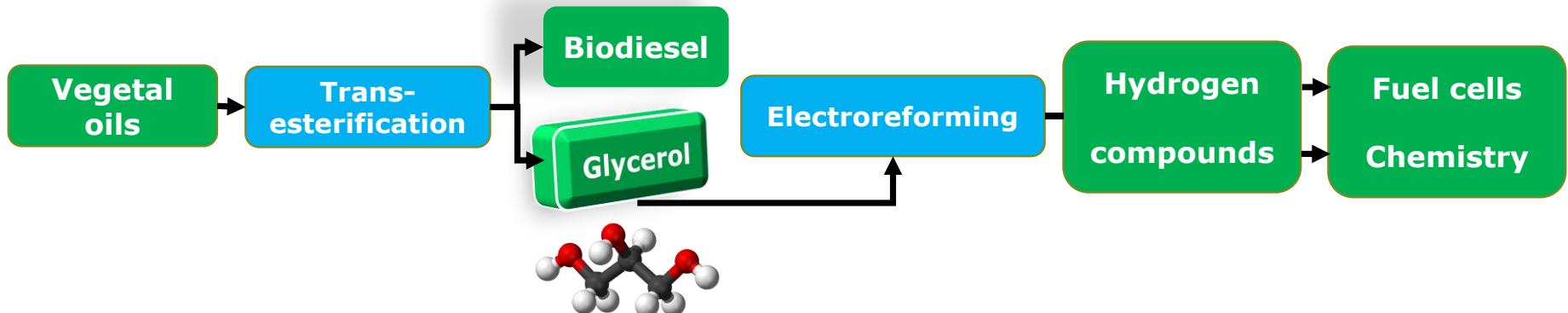
Activation of water at
 $U_{\text{cell}} << 1.23 \text{ V}$

C. Coutanceau, S. Baranton. Electrochemical conversion of alcohols for hydrogen production: a short overview. *WIREs Energy Environ* 2016. doi: 10.1002/wene.193

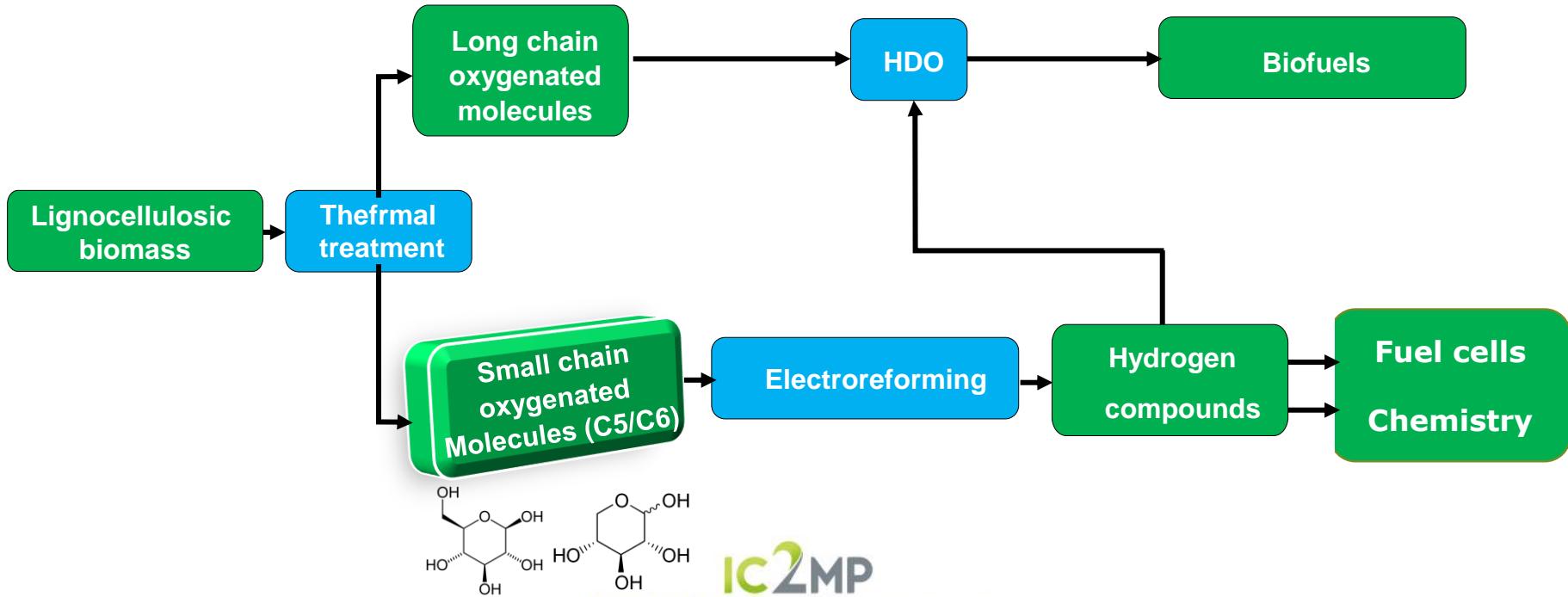
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1st generation biofuels



2nd generation biofuels



Reaction medium

- Molecules such as polyols and sugars more electroreactive in alkaline media
 - Base-catalyzed reaction favoured
 - possibility of using non noble metals
- C-C bond cleavage more difficult in alkaline media at low potentials
 - Enhancement of the selectivity
 - Co-production of hydrogen and high value-added compounds

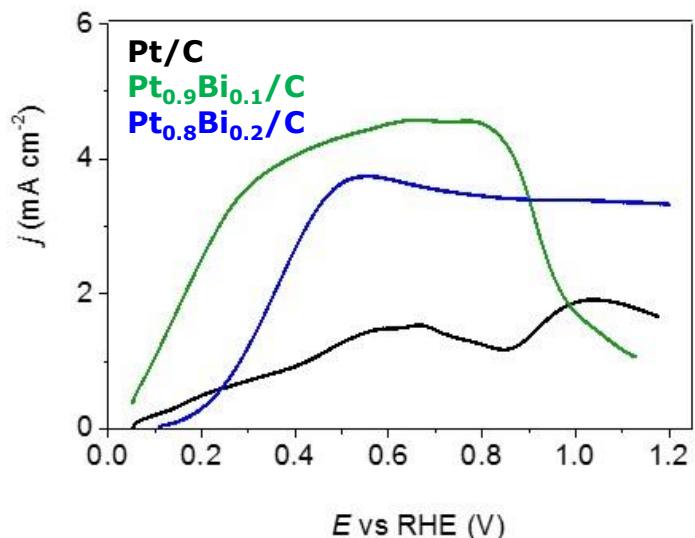
Electrocatalytic materials

PtBi materials known to be catalytically very active towards biomass conversion for a long time

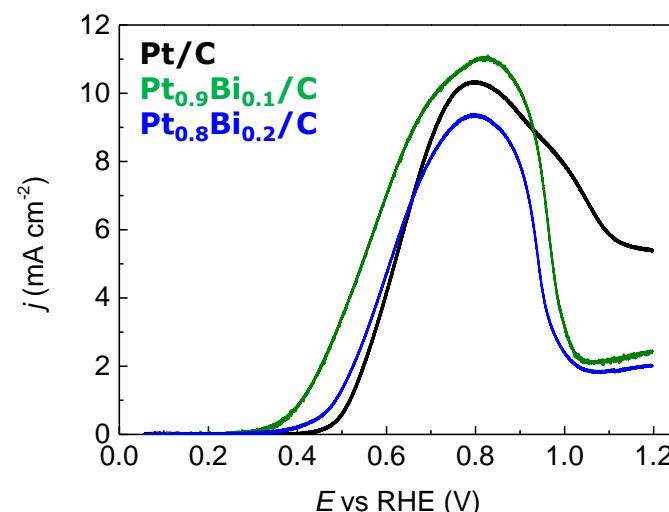
- T. Mallat, A. Baiker, Oxidation of alcohols with molecular oxygen on platinum metal catalysts in aqueous solutions . Catal. Today 19 (1994) 247 – 284
- P. Gallezot, Selective oxidation with air on metal catalysts. Catal. Today 37 (1997) 405 –418

PtBi catalysts are also very electroactive materials for biomass conversion

- M. Simões, S. Baranton, C. Coutanceau. Enhancement of catalytic properties for glycerol electrooxidation on Pt and Pd nanoparticles induced by Bi surface modification . Applied Catalysis B: Environmental 110 (2011) 40 – 49
- J. Cobos-Gonzalez, S. Baranton, C. Coutanceau . Development of Bi-Modified PtPd Nanocatalysts for the Electrochemical Reforming of Polyols into Hydrogen and Value-Added Chemicals ChemElectroChem 3 (2016) 1694–1704
- N. Neha, T. rafaideen, R. B. S. Kouamé, S. Baranton, C. Coutanceau , Remarkably Efficient Carbon-Supported Nanostructured Platinum-Bismuth Catalysts for the Selective Electrooxidation of Glucose and Methyl-Glucoside. Electrocatalysis 12 (2021) 1-14.



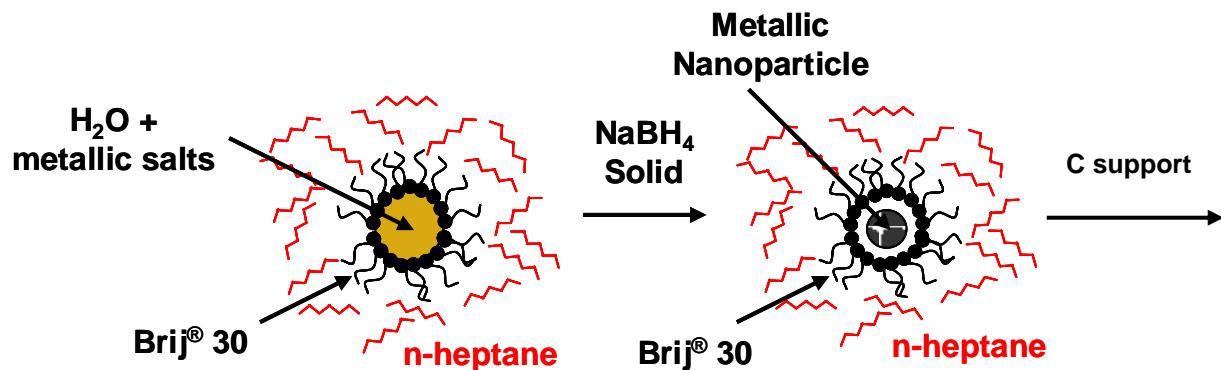
0.1 M glucose electrooxidation in 0.1 M NaOH, 20 °C, scan rate 0,005 V s⁻¹



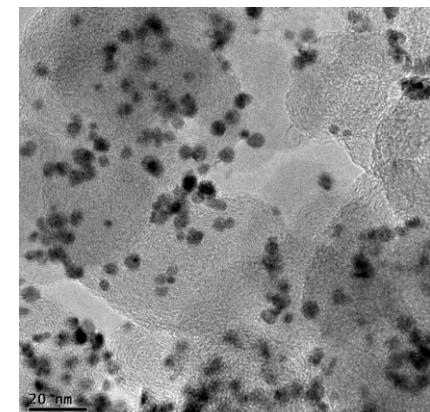
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Synthesis of electrocatalytic materials

“Water in oil” microemulsion synthesis :



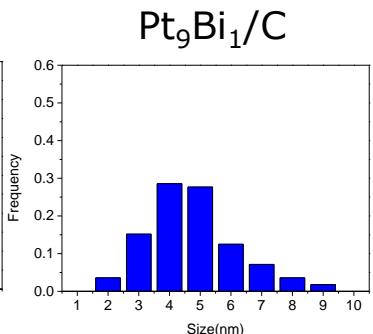
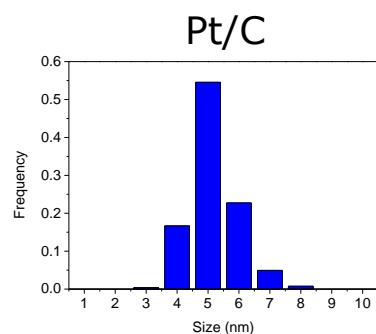
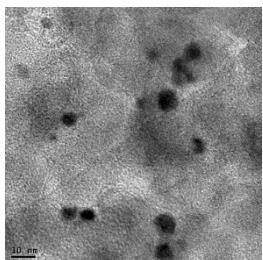
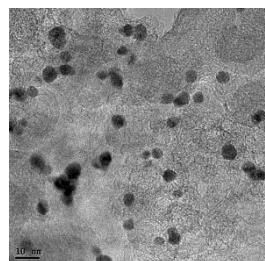
40 wt% M / C



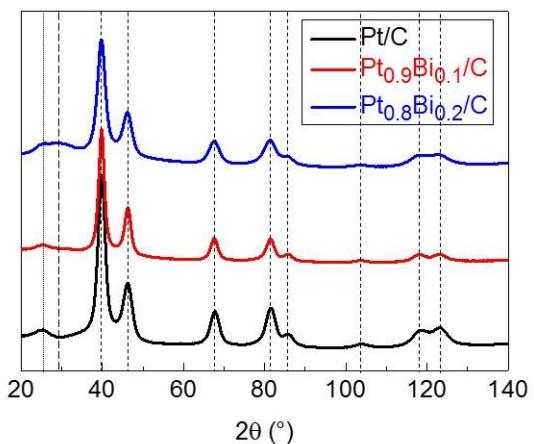
- Easy and rapid to implement
- Formation of nanoparticles from a wide range of metal salts
- Easy cleaning step

Characterization of electrocatalytic materials

TEM

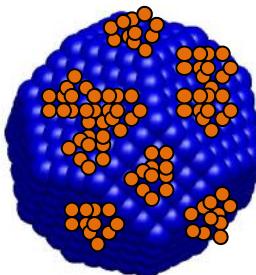


XRD



DRX, AAS, ICP-OES, XPS:

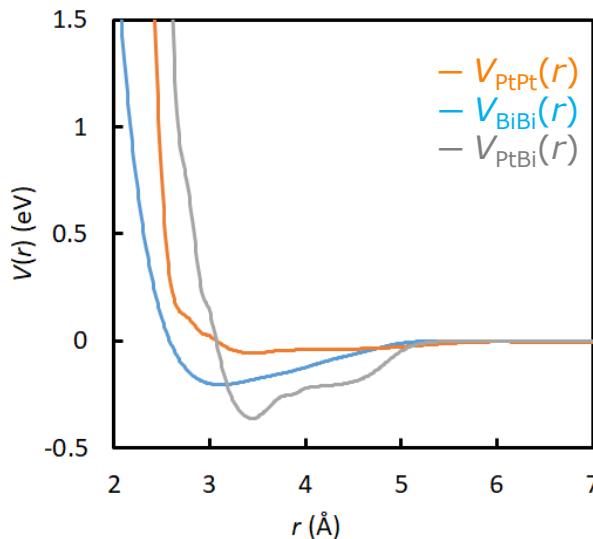
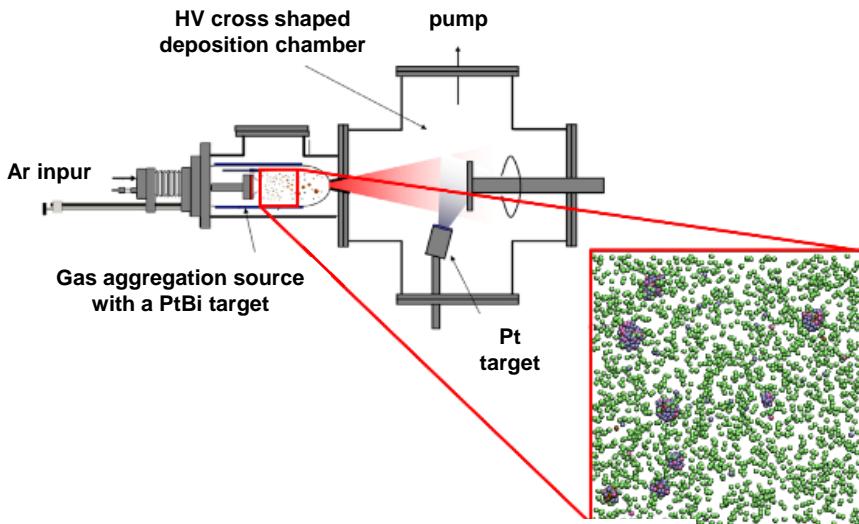
| | Pt/C | Pt ₉ Bi ₁ /C | | Pt ₈ Bi ₂ /C | |
|----------------------------|--------|------------------------------------|------------------------------------|------------------------------------|--------------------------|
| Comp. ICP-OES (at%) | 100 | Pt | Bi | Pt | Bi |
| | | 92 | 8 | 84 | 16 |
| Comp. AAS (at%) | 100 | Pt | Bi | Pt | Bi |
| | | 88.2 | 11.8 | 78.2 | 21.8 |
| d (nm) | 5.2 | 4.7 | | 4.7 | |
| L_v (nm) | 3.5 | 4.3 | | 3.1 | |
| a (nm) | 0.3916 | 0.3919 | | 0.3926 | |
| Comp. XPS (at%) | | Pt ⁰ : 79 | Bi _{total} : 21 | Pt ⁰ : 72 | Bi _{total} : 28 |
| | | | Bi(OH) ₂ : 72 | | Bi ⁰ : 9 |
| | | | Bi(OH) ₃ : 22 | | Bi(OH) ₂ : 34 |
| | | | Bi ₂ O ₄ : 6 | | Bi(OH) ₃ : 51 |
| | | | | | Bi ₂ O : 6 |



- M. Simões, S. Baranton, C. Coutanceau. Enhancement of catalytic properties for glycerol electrooxidation on Pt and Pd nanoparticles induced by Bi surface modification . *Applied Catalysis B: Environmental* 110 (2011) 40 – 49
- B. S. R. Kouamé, S. Baranton, C. Canaff, P. Brault, W. Chamorro-Coral, A. Caillard, K. De Oliveira Vigier, C. Coutanceau. Insights on the unique electrocatalytic behavior of PtBi/C materials. *Electrochim. Acta* 329 (2020) 135161.

Molecular dynamics

For more information: pascal.brault@univ-orleans.fr
GREMI



Interaction potentials as a function of the interatomic distance (r) used in the MD simulations.

Conditions for MDs calculation:

- Growth of $\text{Pt}_n\text{Bi}_{500-n}$ nanoparticles ($n \leq 500$) in GAS configuration
- To mimic the synthesis by wet chemistry
 - T maintained around 300 K (with low fluctuations) using a Berendsen thermostat.
 - The energy of clusters bond formation after collisions is transported and dissipated by the Ar atoms acting as the solvent in the case of the synthesis of nanoparticles by wet chemistry.

- Pt-Bi bond strength > Pt-Pt and Bi-Bi bond strengths
- Pt-Bi equilibrium distance is larger than the Pt-Pt distance

=> Bi should be located on the outermost surface

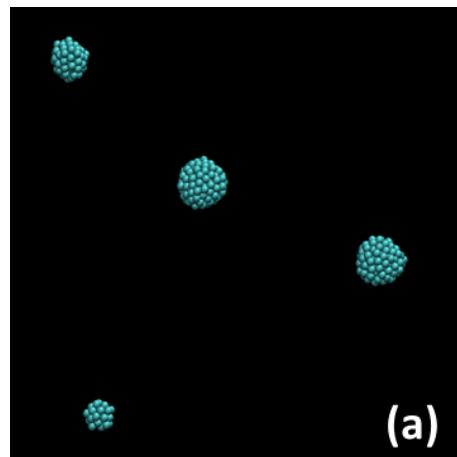
=> strong electronic interaction between Pt and Bi

B. S. R. Kouamé, S. Baranton, C. Canaff, P. Brault, W. Chamorro-Coral, A. Caillard, K. De Oliveira Vigier, C. Coutanceau. Insights on the unique electrocatalytic behavior of PtBi/C materials. *Electrochim. Acta* 329 (2020) 135161.

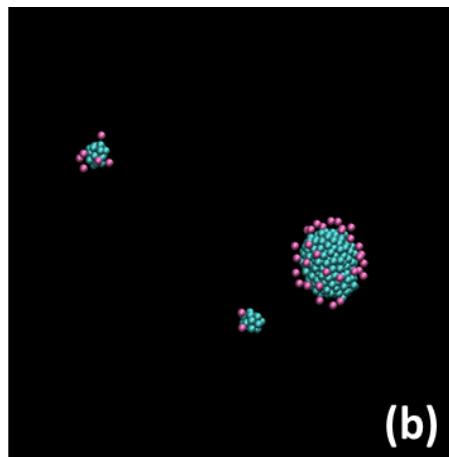
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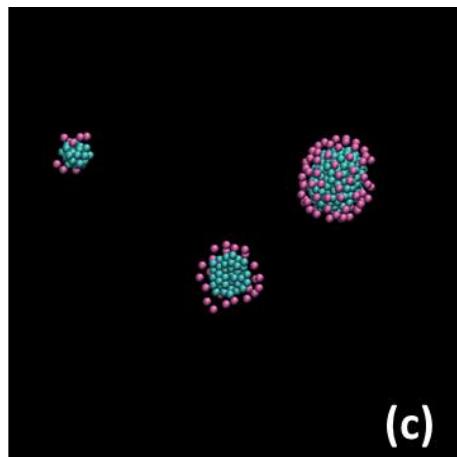
Pt



Pt₉Bi₁



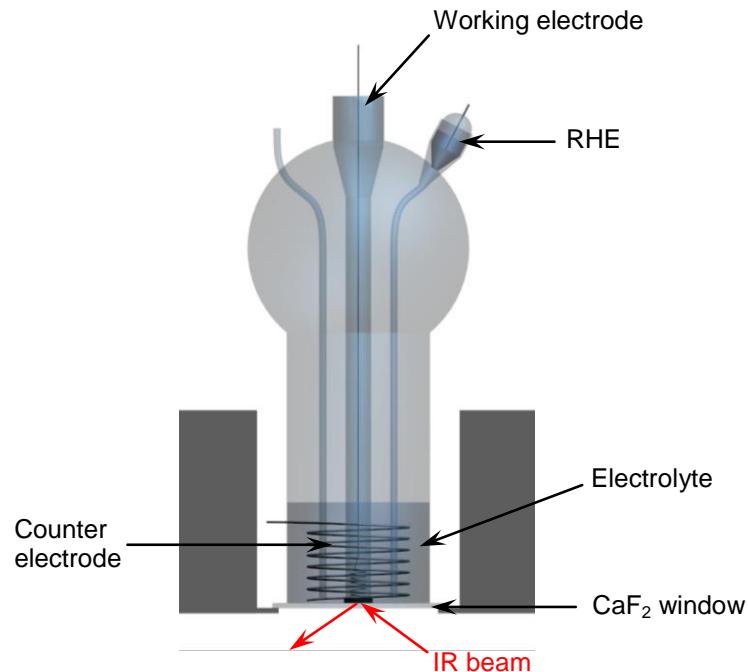
Pt₈Bi₂



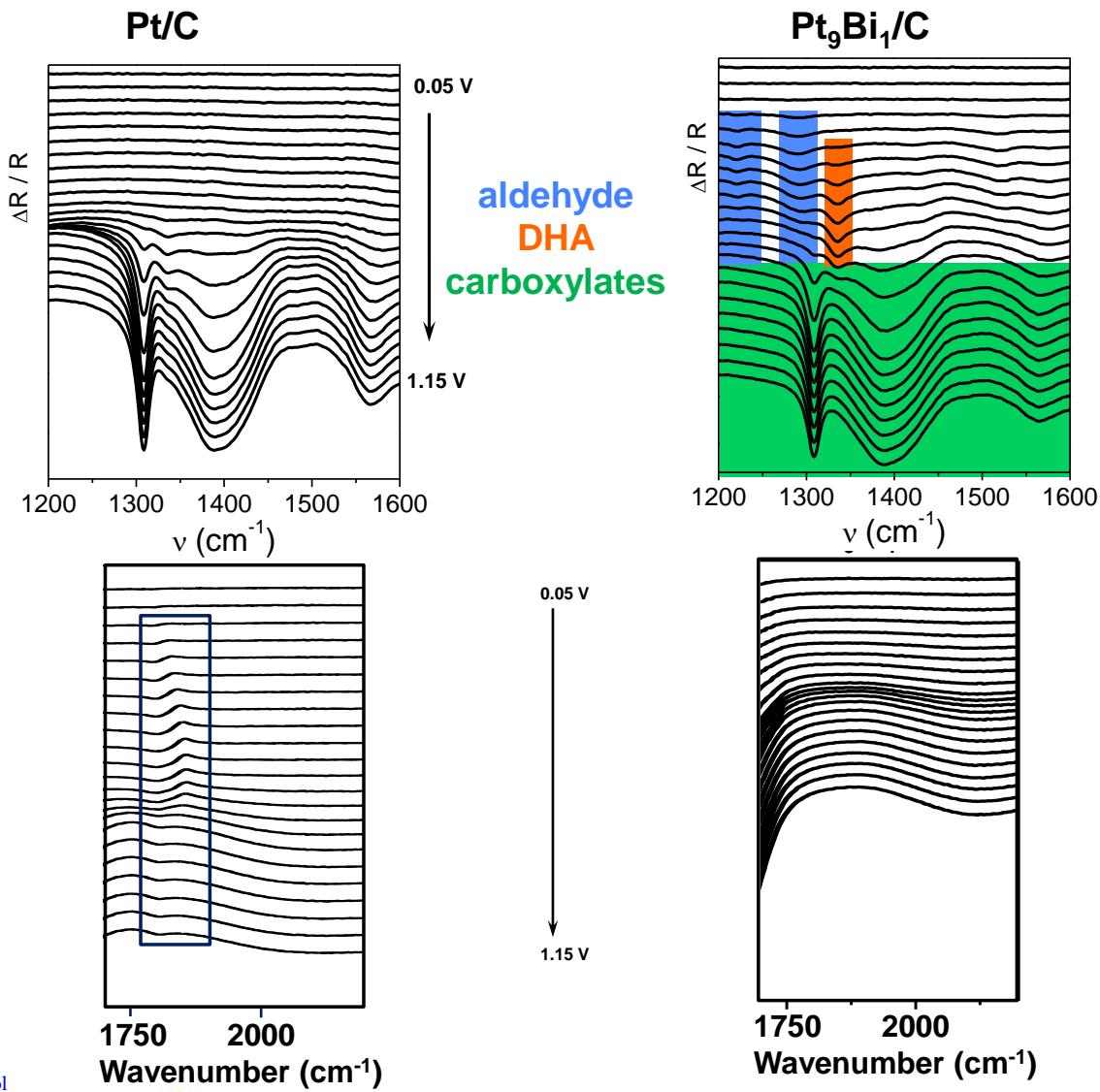
Snapshots at 20 ns for all considered Pt_{1-x}Bi_x atomic compositions

- Bi atoms are always decorating Pt core clusters
- The Pt core is crystalline
- Each cluster is stoichiometric: Pt/Bi atomic composition globally and locally preserved
- For 20 at. % Bi (Pt_{0.8}Bi_{0.2}), the Pt core cluster is almost fully hidden by Bi atoms

Selectivity by in situ FTIRs: Glycerol

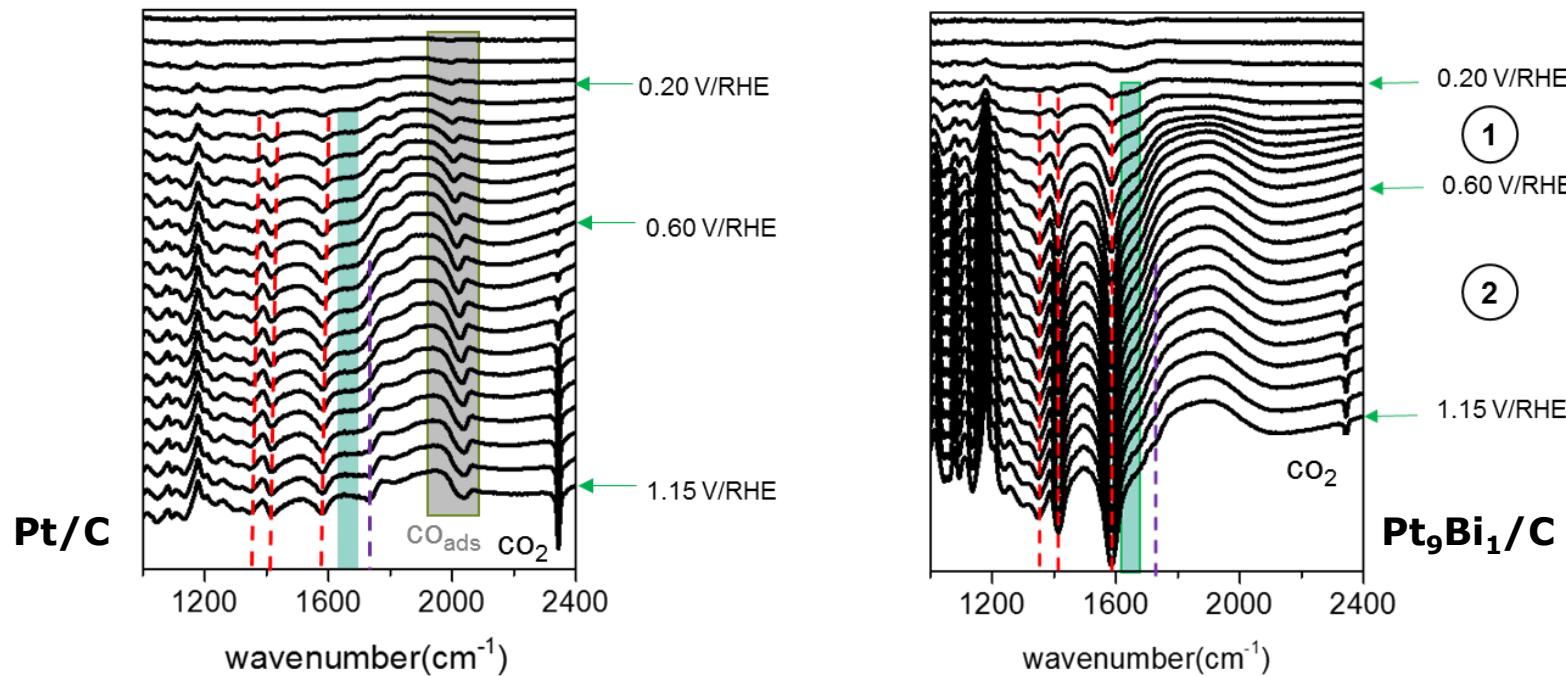


In situ IR electrochemical cell

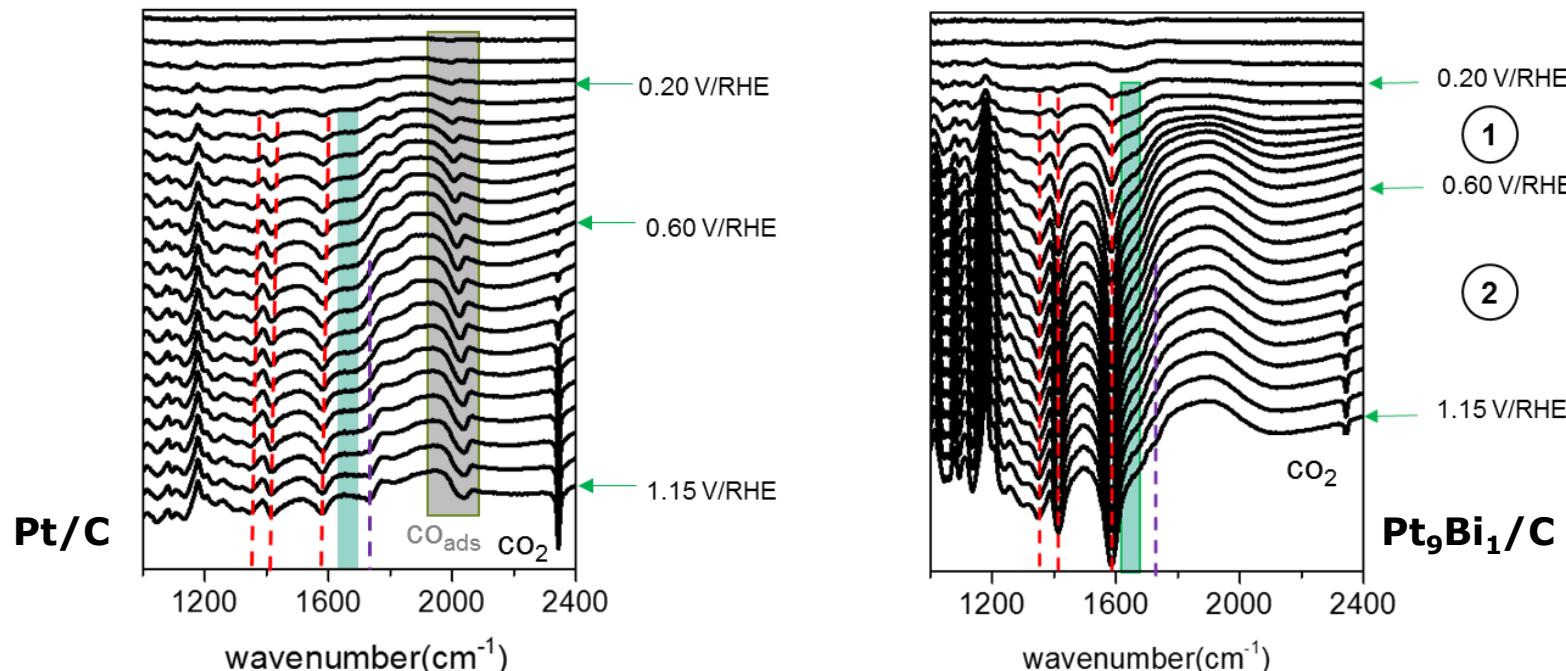


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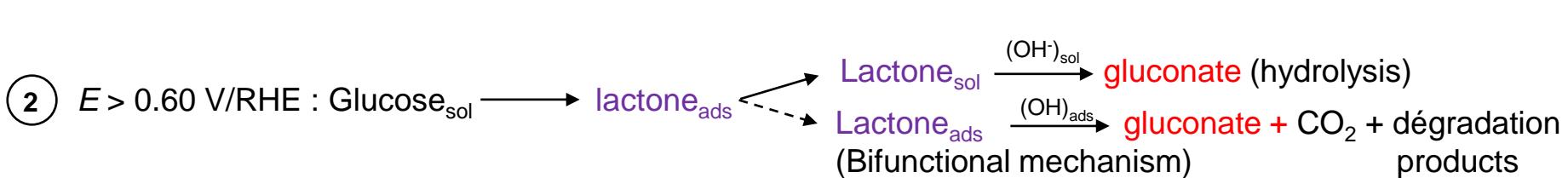
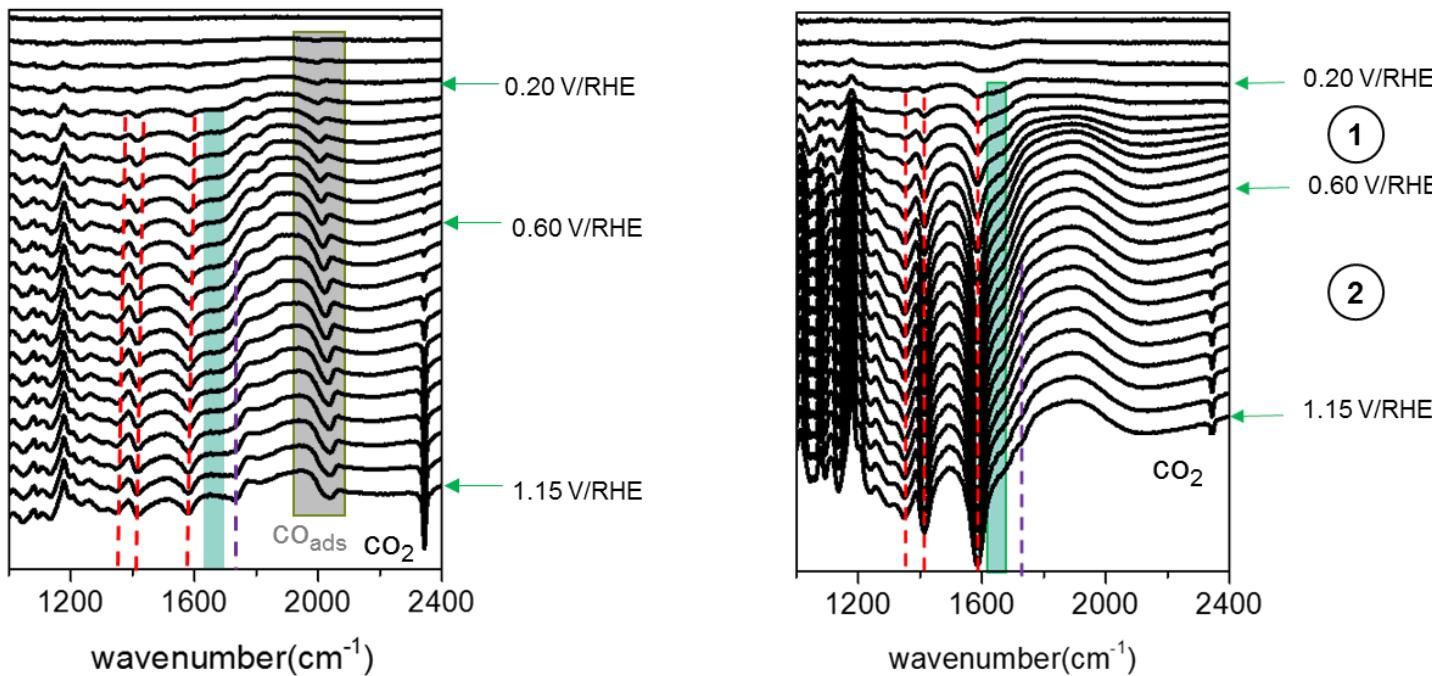
Selectivity by in situ FTIR: glucose oxidation



Selectivity by in situ FTIR: glucose oxidation

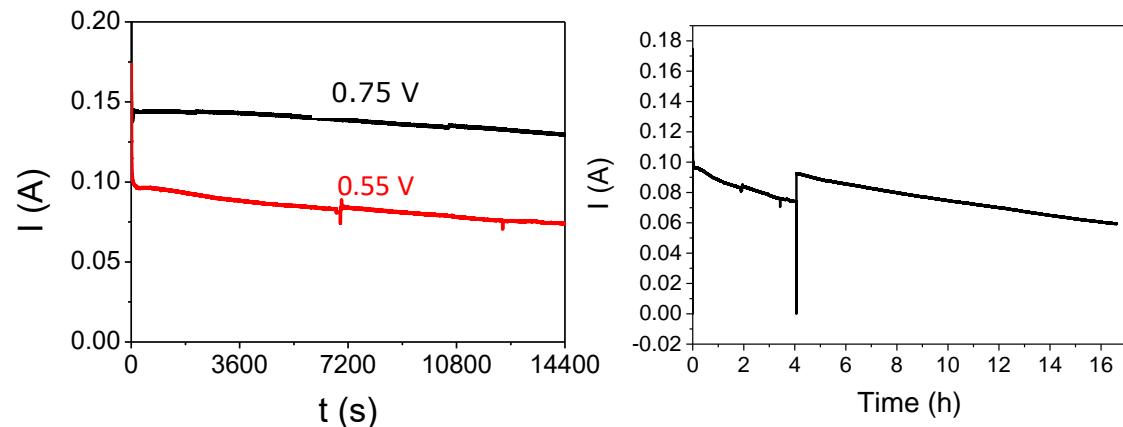
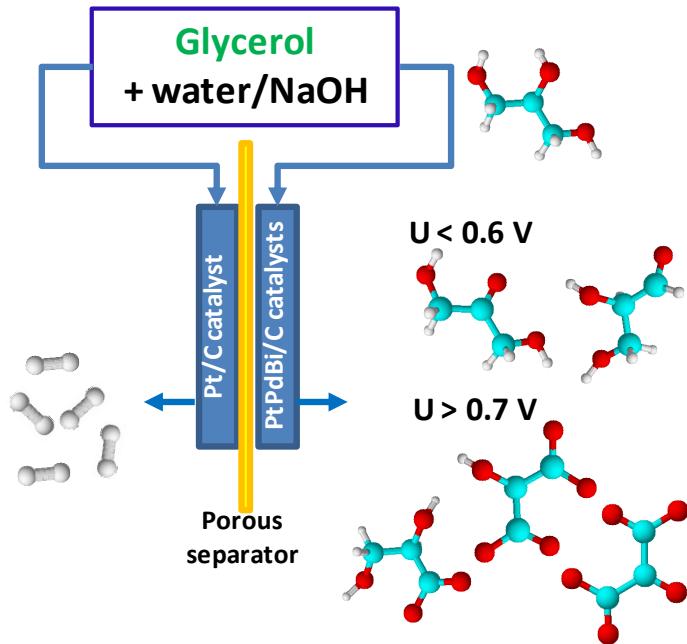


Selectivity by in situ FTIR: glucose oxidation



Electroreforming of oxygenated compounds from biomass

Glycerol electroconversion



25 cm⁻² electrolysis cell fitted with a Pt/C cathode and a Pt₉Bi₁/anode (electrodes: 1.6 mg cm_{metal}⁻²); 2 M glycerol + 0.5 M NaOH, 20 °C flow rate = 2 mL min⁻¹

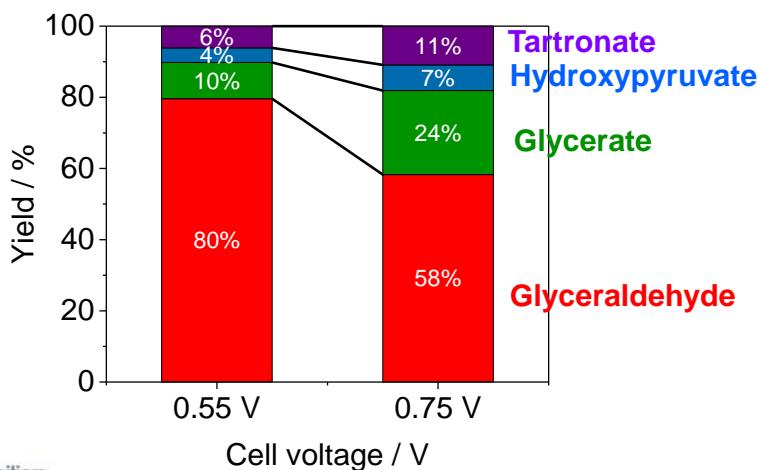
$$W_e \left(\text{in } \frac{\text{kWh}}{\text{Nm}^3} \right) W_e = \frac{n_e F}{3600 V_m \times 10^3} U_{\text{cell}}(j) \approx 2.364 U_{\text{cell}}(j)$$

At 0.55 V: $W_e = 1.3 \text{ kWh sm}_{\text{H}_2}^{-3}$

At 0.75 V: $W_e = 1.77 \text{ kWh sm}_{\text{H}_2}^{-3}$

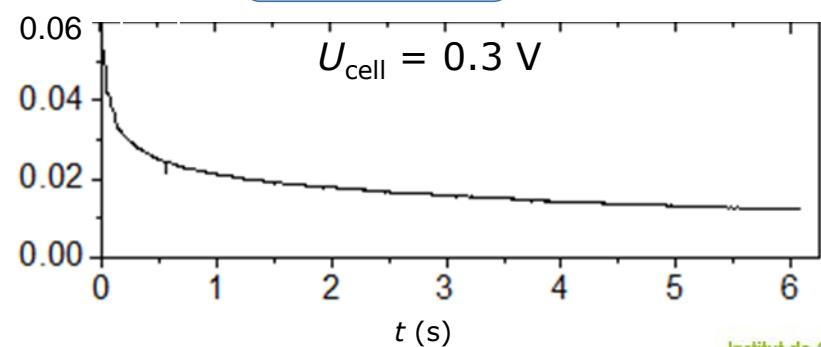
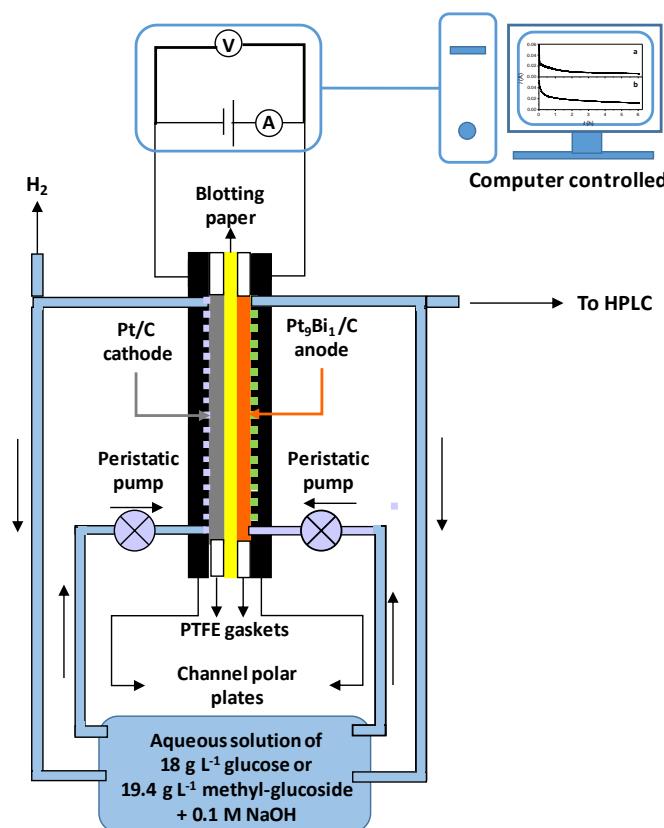
Water electrolysis: 3.8 – 4.3 kWh / Nm³

Reaction product distribution (Except dihydroxyacetone)

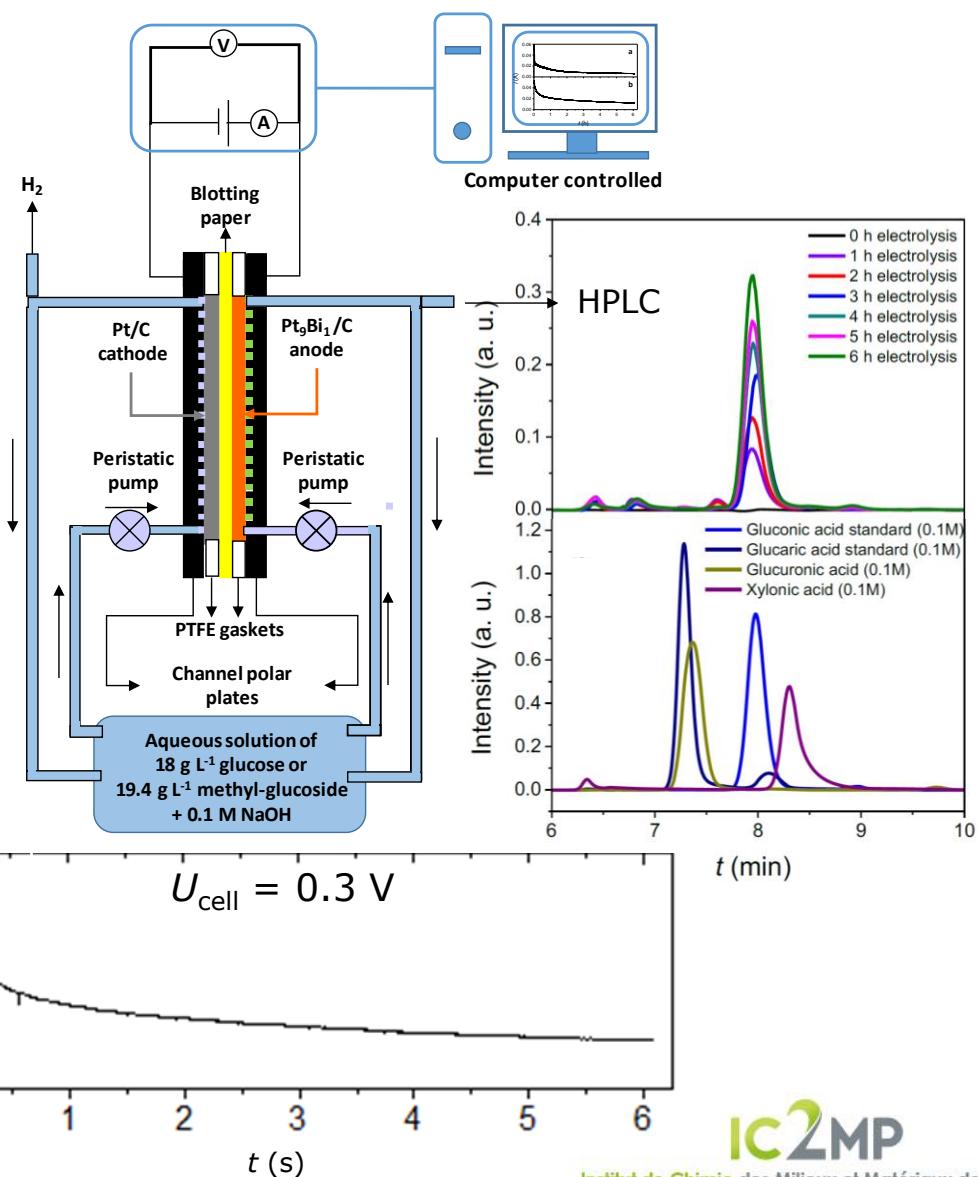


J. Cobos-Gonzalez, S. Baranton, C. Coutanceau . Development of Bi-Modified PtPd Nanocatalysts for the Electrochemical Reforming of Polyols into Hydrogen and Value-Added Chemicals
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Glucose electroconversion

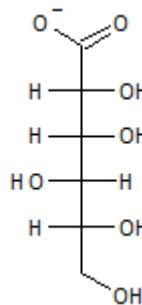
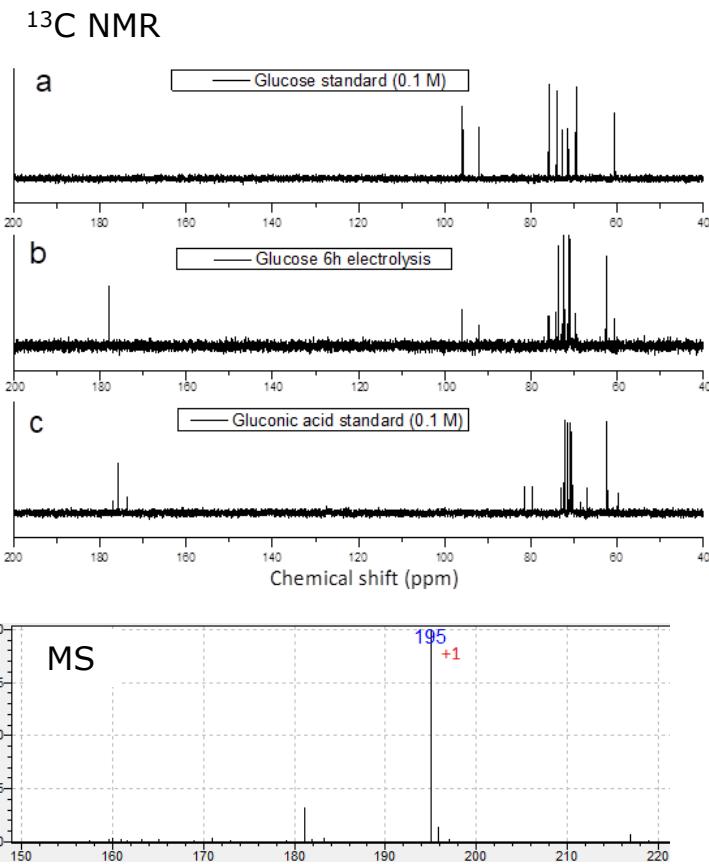
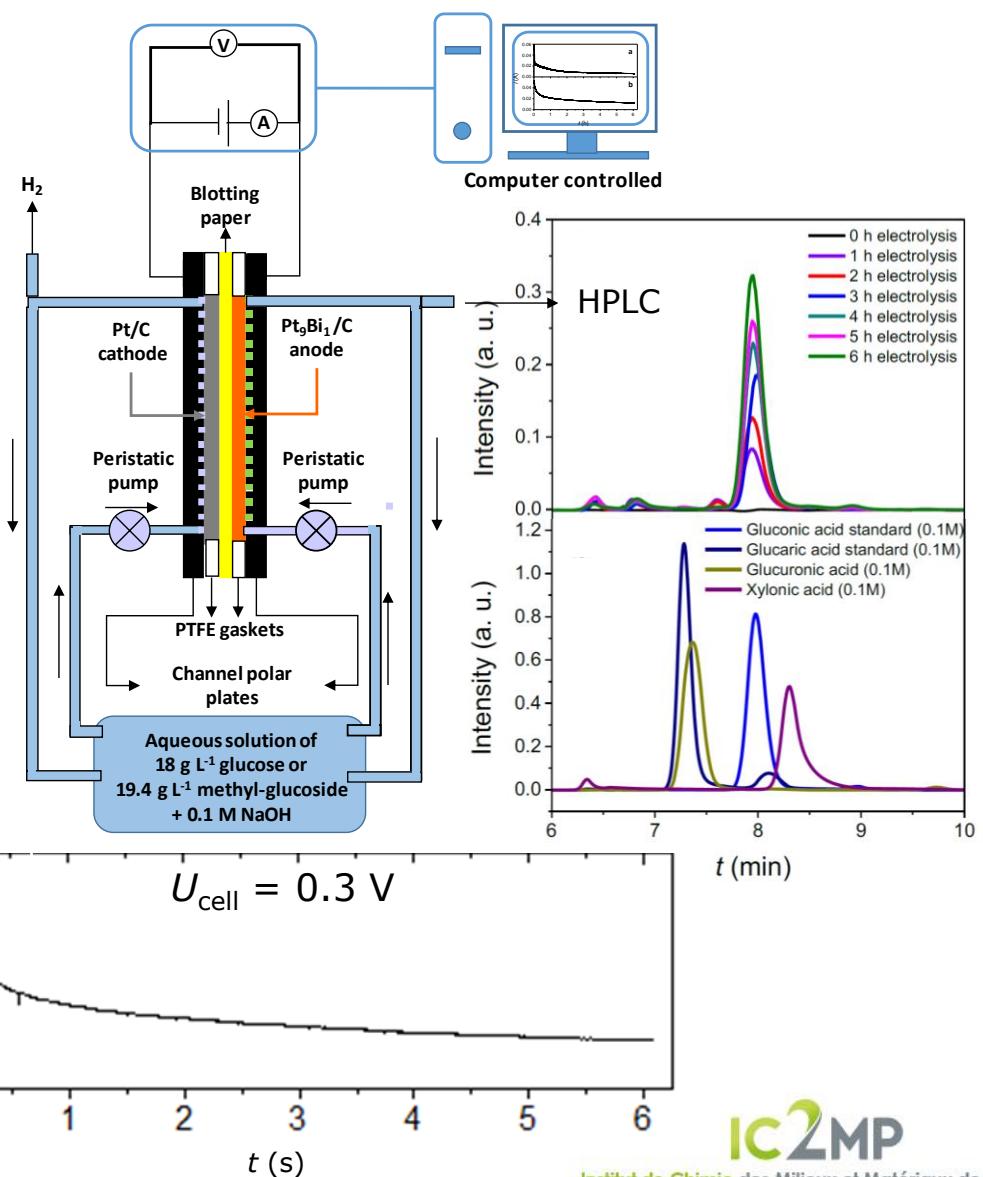


Glucose electroconversion

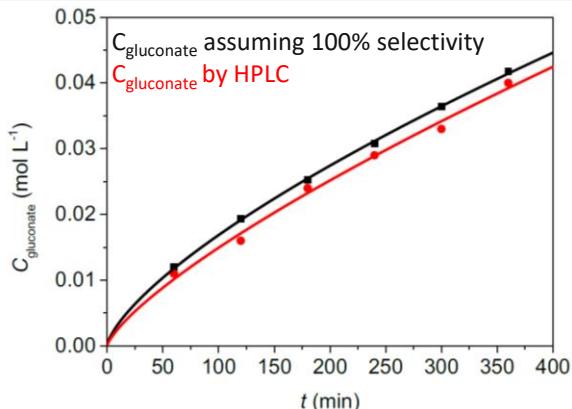


Electroreforming of oxygenated compounds from biomass

Glucose electroconversion



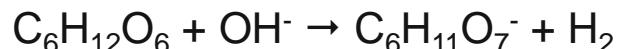
Electroreforming of oxygenated compounds from biomass



Selectivity ~100 %; Faradaic yield ~100 %; ~40 % conversion

At 0.30 V: $W_e = 0.71 \text{ kWh Nm}_{\text{H}_2}^{-3}$
 Water electrolysis: 3.8 – 4.3 kWh / Nm³

Energy cost at 0.3 V: 1 molecule of H₂ is evolved by molecule of gluconate produced



The production of 1 ton sodium gluconate is then accompanied with the evolution of 9 kg H₂

The specific electrical energy consumed at 0.3 V corresponds to ca. 8.05 kWh kg_{H₂}⁻¹

Assuming a mean electricity cost of ca. 0.15 €/kWh in Europe, it corresponds to 11 €



Less than 3% of commercial prices for industrially produced sodium gluconate

600 to 750 US \$, i.e. 750 to 950 CAD per ton (Dezhou Huiyang Biotechnology Co., Ltd., Wuxi Fengmin Environmental Technology Development Co., Ltd., etc.).

Low current densities

Low hydrogen production rate

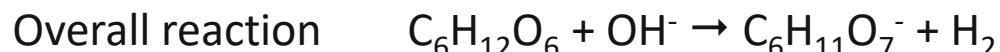
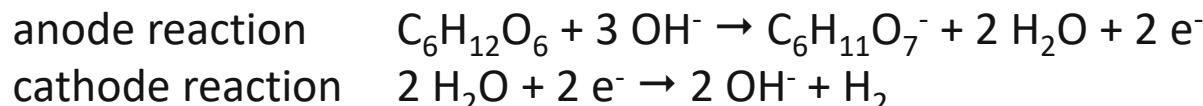


Problem of hydroxyl ions migration from cathode to the anode

Reaction of sugars/reaction products at the cathode

=> Use of an AEM + ionomer

Increase of sugars/polyols concentrations



=> increase of the hydroxyl ions concentration => problem of molecules stability

PGM based catalyst: high cost, strategic materials, availability, etc.

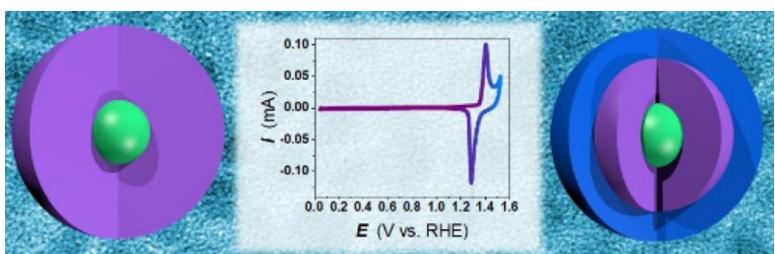
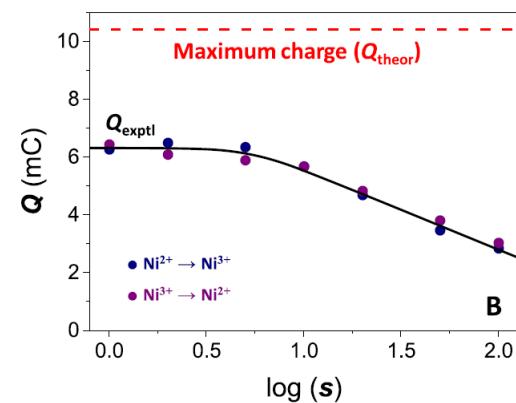
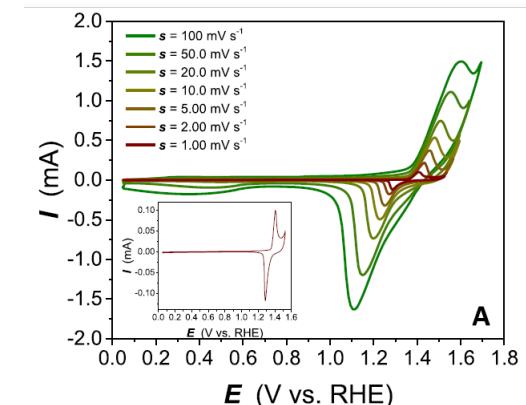
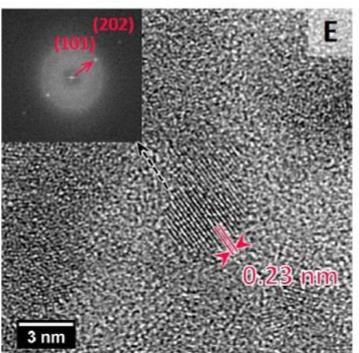
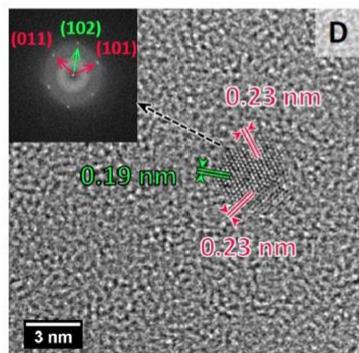
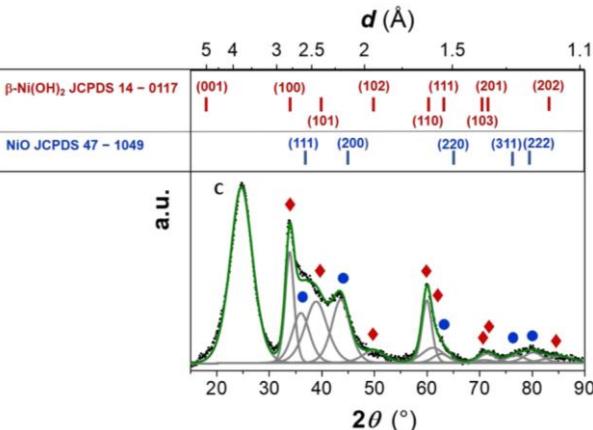
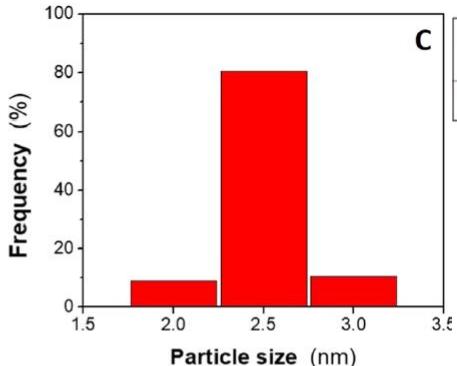
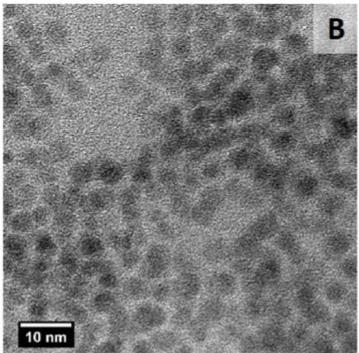
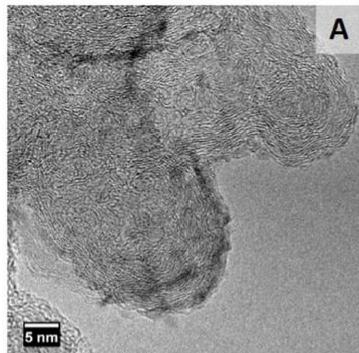


=> development of non-PGM catalysts, electroactive at a potential as low as possible and allowing achieving high current densities

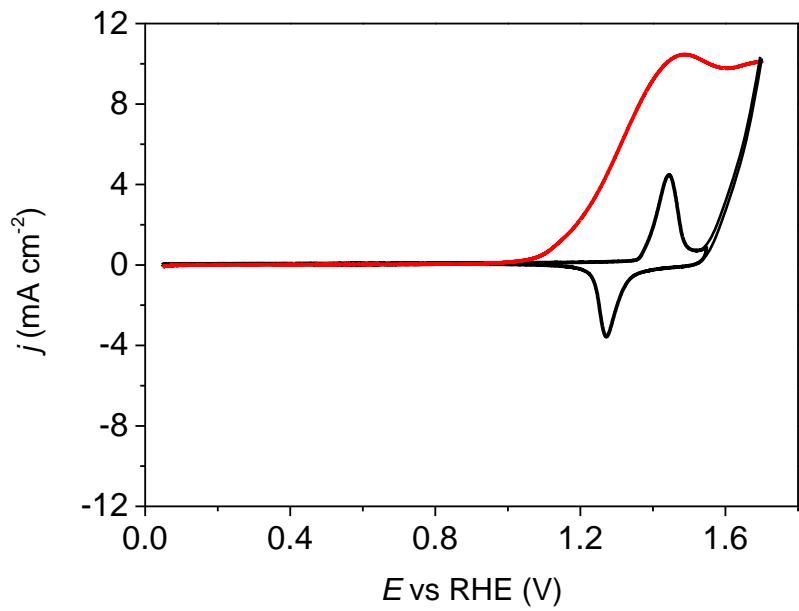
=> Nickel is known to be an active materials for alcohol electrooxidation



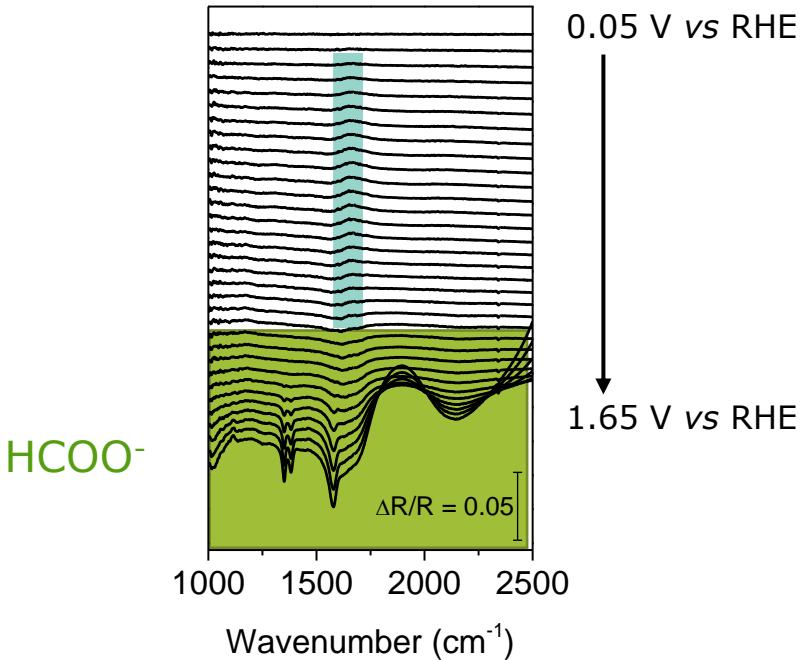
Synthesis on Ni(OH)_2 nanoparticles by the water in oil microemulsion method



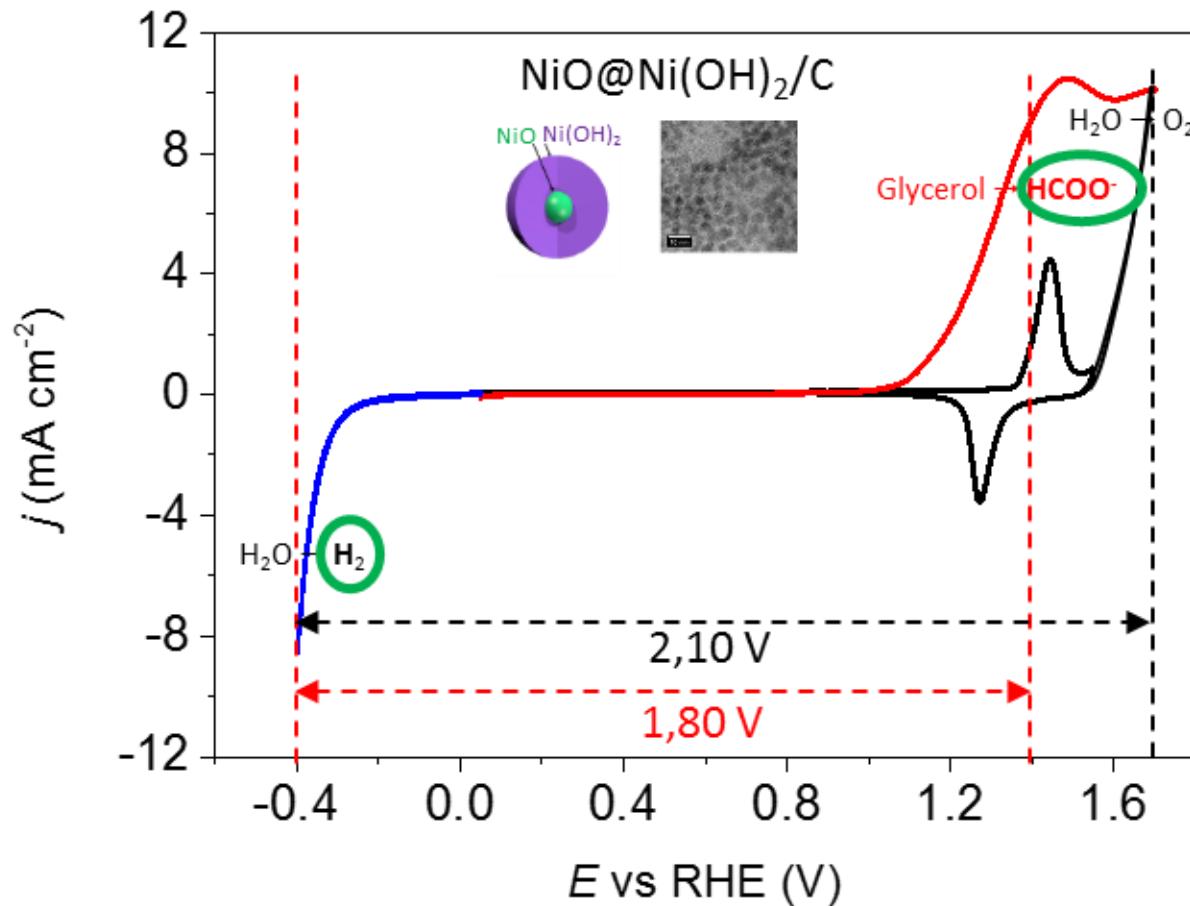
Activity and selectivity of Ni(OH)_2 nanoparticles towards glycerol electrooxidation



Cyclic voltammetry of a Ni/C catalysts recorded in 0.1 M NaOH (black line) and $0.1 \text{ M NaOH} + 0.1 \text{ M glycerol}$ (red line) media (scan rate = 10 mV s^{-1} , metal loading = $50 \mu\text{g cm}^{-2}$, $S_{\text{geom}} = 0.071 \text{ cm}^2$, $T = 20^\circ \text{ C}$)



Activity and selectivity of Ni(OH)₂ nanoparticles towards glycerol electrooxidation



Both H₂ and HCOO⁻ can serve as fuels in low temperature fuel cells

The electroreforming of oxygenated organic molecules allows decreasing the electrolysis cell voltage for hydrogen production

It is better to use wastes from bio-industries such as glycerol, C5 and C6 sugars

=> decrease of the OPEX for biofuels and hydrogen production

But the kinetics of electroreforming reaction are very low on PGM-based catalysts, and more PGM are needed to enhance the reaction rate

=> Increase of the CAPEX

Increase of sugars/polyols and hydroxyl ions diffusion towards catalytic sites

Development of non-PGM based catalysts (Ni-based)

=> decrease of both the CAPEX and the OPEX

Thank you for your attention



Nouvelle Aquitaine
County Council

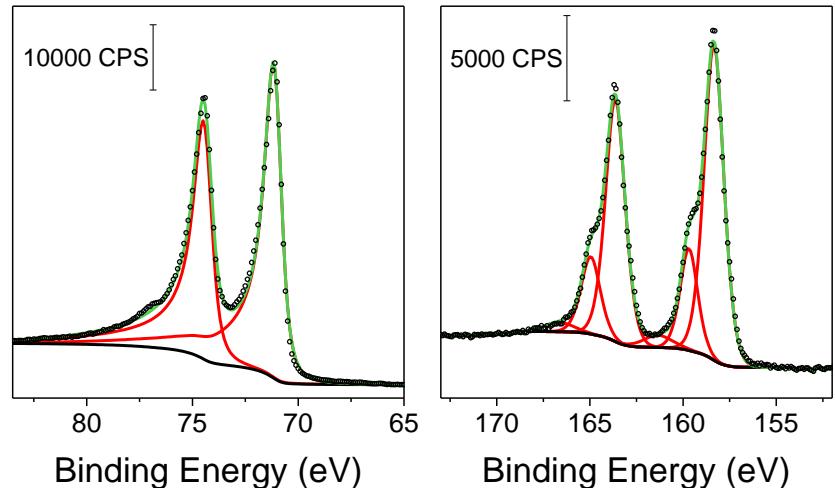


UNION EUROPÉENNE
Fonds Européen de Développement Régional
European commission
(ERDF)

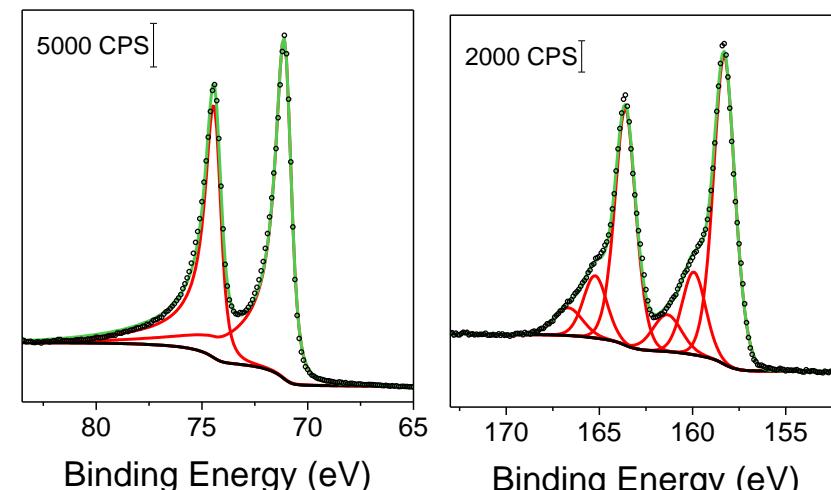
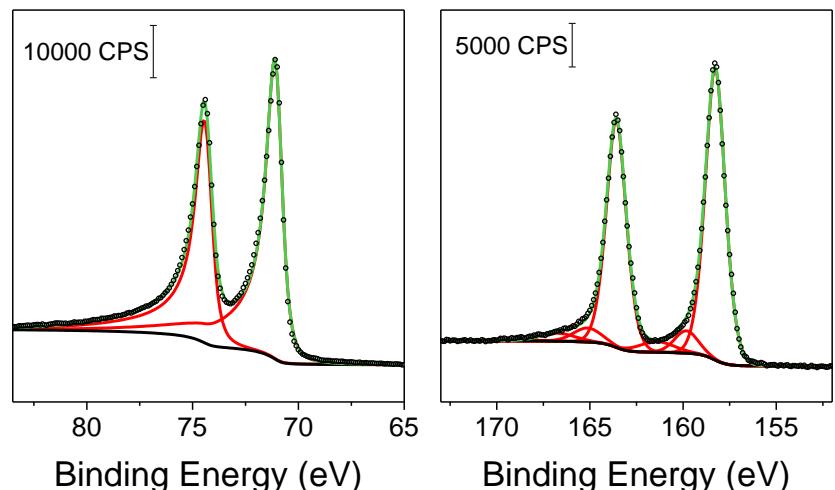
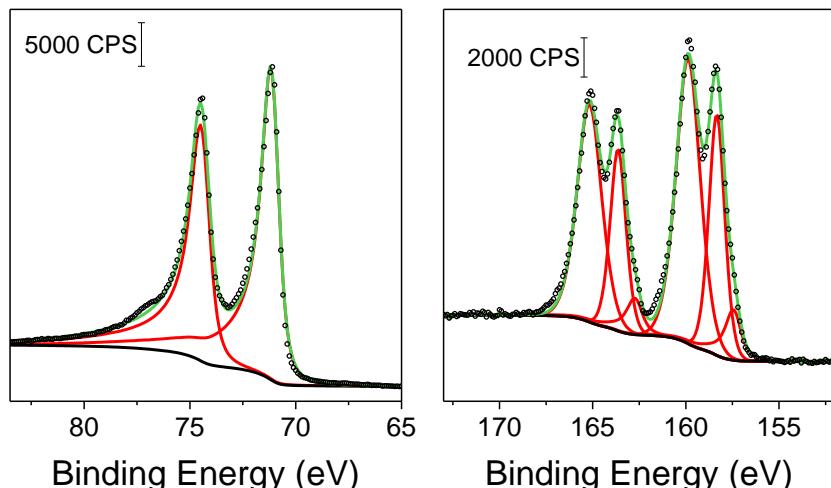


National Agency
for Research

Fresh Pt₉Bi₁/C



Fresh Pt₈Bi₂/C



~ Pt⁰ (79%), ↑ Bi²⁺ (87%), ↓ Bi³⁺ (8%), ↓ Bi⁴⁺ (5%)

~ Pt⁰ (71%), ↓ Bi⁰, ↑ Bi²⁺ (69%), ↓ Bi³⁺ (20%), ↑ Bi⁴⁺ (11%)

